

```
>> compare_methods_4
```

```
Part a:
```

```
Given vertical deflection = 0.200 m  
Computed weight of object = 640.743 N
```

```
Part b:
```

```
Given object's weight = 250.000 N
```

```
Results for Scale Deflection ==> Bisection Secant Matlab's FZERO  
  
A zero occurs at x = 0.1099892 0.1099892 0.1099892 m  
The value of f(x) is = 0.0000001 -0.0000000 0.0000000 N  
# of function evaluations = 31 8 10
```

COMPARE\_METHODS\_4.M Compare three root finding methods for relative efficiency

This project involves comparing the efficiency of the Bisection and Secant Methods relative to Matlab's built-in FZERO function for finding the real roots of nonlinear equations.

This code also illustrates the difference between explicit and implicit equations. An expression that relates the weight,  $W$ , and vertical deflection,  $x$ , of a particular scale arrangement was derived in the problem description. Given  $x$ ,  $W$  can be easily determined via an explicit evaluation of the given equation. However, if  $W$  is given, we need to use a root finding routine to evaluate  $x$ , since the relationship,  $x(W)$ , is implicit -- that is, we can't easily write the equation in the form of  $x = f(W)$ . This implicit equation is used to illustrate the relative efficiency of the various root finding methods:

```
Bisection Method          -- bisection.m
Secant Method             -- secant.m
Matlab's built-in function -- fzero.m
```

The function evaluations are done using anonymous functions since the relationships are relatively simple.

File prepared by J. R. White, UMass-Lowell (last update: Nov. 2017)

```
clear all, close all, nfig = 0;
```

```
base design parameters
```

```
a = 0.15;  b = 0.05;          % geometry parameters (m)
K = 2800;   % spring constants (N/m)
Lo = sqrt(a*a + b*b);        % unstretched spring length
```

```
anonymous functions (only scalar arithmetic is used here -- so no dots needed)
```

```
Lx = @(x) sqrt(a*a + (b + x)^2); % explicit relation for L(x)
Wx = @(x) (2*K/Lx(x))*(Lx(x) - Lo)*(b + x); % explicit relation for W(x)
```

```
Part a: Find weight of object given deflection, x (explicit equation)
```

```
xa = 0.2;  Wa = Wx(xa); % given deflection and computed weight
fprintf('\n Part a: \n')
fprintf(' Given vertical deflection = %8.3f m \n ', xa)
fprintf(' Computed weight of object = %8.3f N \n ', Wa)
```

```
Part b: Find deflection of scale given the object's weight, W (implicit equation)
```

```
Wb = 250; % object's weight (N)
fx = @(x) Wb - Wx(x); % implicit relation for f(x) = W - W(x) = 0
fprintf('\n\n Part b: \n')
fprintf(' Given object's weight = %8.3f N \n ', Wb)
```

```
call the various root finding methods and tabulate the results
```

```
M = 50;  tol = 1e-6;  display = 0;  lb = 0;  ub = 0.2;
[xb1, k1] = bisection(fx, lb, ub, tol, M, display);  f1 = fx(xb1);
[xb2, k2] = secant(fx, lb, ub, tol, M, display);    f2 = fx(xb2);
[xb3, f3, flag, output] = fzero(fx, [lb ub]);
```

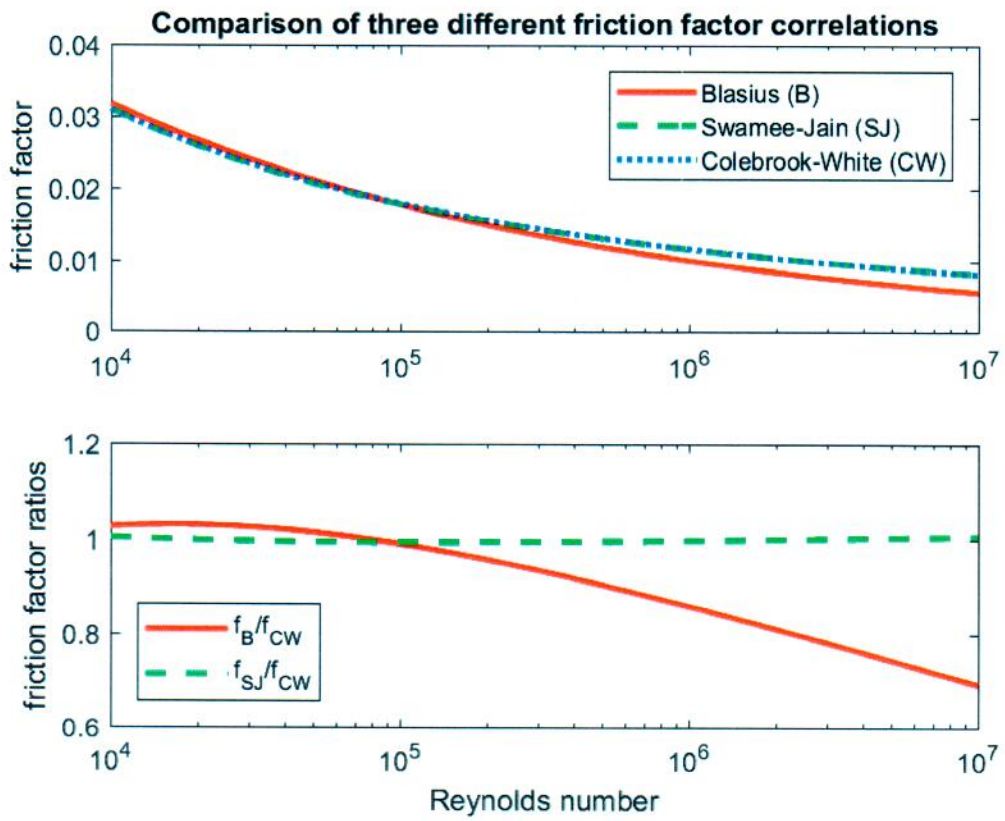
```
fprintf('\n Results for Scale Deflection ==> Bisection Secant Matlab's
```

```
FZERO \n\n')
```

```
fprintf(' A zero occurs at x = %12.7f %12.7f %12.7f m\n', ...
```

```
        xb1,xb2,xb3)
fprintf(' The value of f(x) is =          %12.7f %12.7f %12.7f N\n',f1,f2,f3)
fprintf(' # of function evaluations =    %6i %12i  %12i\n', ...
        k1+2,k2+2,output.funcCount)
```

```
end of problem
```



>> fricf\_1

Comparison of Three Friction Factor Correlations for Smooth Pipes  
(fB -> Blasius eqn, fSJ -> Swamee-Jain, & fCW -> Colebrook-White correlation)

Re	fCW	fB	fB/fCW	fSJ	fSJ/fCW
1.00e+04	0.03089	0.03164	1.024	0.03097	1.003
1.26e+04	0.02908	0.02987	1.027	0.02910	1.001
1.58e+04	0.02743	0.02820	1.028	0.02739	0.999
2.00e+04	0.02590	0.02662	1.028	0.02583	0.997
2.51e+04	0.02450	0.02513	1.026	0.02440	0.996
3.16e+04	0.02320	0.02373	1.023	0.02308	0.995
3.98e+04	0.02200	0.02240	1.018	0.02187	0.994
5.01e+04	0.02088	0.02115	1.013	0.02075	0.994
6.31e+04	0.01985	0.01996	1.006	0.01971	0.993
7.94e+04	0.01889	0.01885	0.998	0.01875	0.993
1.00e+05	0.01799	0.01779	0.989	0.01786	0.993
1.26e+05	0.01716	0.01680	0.979	0.01703	0.993
1.58e+05	0.01638	0.01586	0.968	0.01626	0.993
2.00e+05	0.01565	0.01497	0.957	0.01554	0.993
2.51e+05	0.01496	0.01413	0.945	0.01486	0.993
3.16e+05	0.01432	0.01334	0.932	0.01423	0.994
3.98e+05	0.01372	0.01260	0.918	0.01364	0.994
5.01e+05	0.01315	0.01189	0.904	0.01308	0.995
6.31e+05	0.01262	0.01123	0.889	0.01256	0.995
7.94e+05	0.01212	0.01060	0.874	0.01207	0.996
1.00e+06	0.01165	0.01001	0.859	0.01161	0.997
1.26e+06	0.01120	0.00945	0.843	0.01117	0.997
1.58e+06	0.01078	0.00892	0.827	0.01076	0.998
2.00e+06	0.01038	0.00842	0.811	0.01037	0.999
2.51e+06	0.01000	0.00795	0.795	0.01000	1.000
3.16e+06	0.00964	0.00750	0.778	0.00965	1.000
3.98e+06	0.00930	0.00708	0.762	0.00931	1.001
5.01e+06	0.00898	0.00669	0.745	0.00900	1.002
6.31e+06	0.00867	0.00631	0.728	0.00870	1.003
7.94e+06	0.00838	0.00596	0.711	0.00841	1.004
1.00e+07	0.00810	0.00563	0.694	0.00814	1.005



```

FRICF_1.M   Compare three different Friction Factor Correlations
            for turbulent flow in smooth pipes
            (An example that requires finding roots of nonlinear expressions)

```

```

This project involves comparing the friction factor using three different
correlations for a range of Reynolds numbers. One implicit expression for f is
given by the Colebrook-White equation:

```

$$1/\sqrt{f} = 2.0 \cdot \log_{10}(\text{Re} \cdot \sqrt{f}) - 0.8$$

```

Two other commonly used explicit relationships are:

```

```
Blasius equation:      f = 0.3164/Re^(1/4)
```

```
Swamee-Jain correlation: f = 0.25/(log10(5.74/Re^0.9))^2
```

```

where all three correlations are for turbulent flow in smooth pipes. This
program computes and compares these correlations for a wide range of Reynolds
numbers.

```

```

Matlab's FZERO root finding routine is used with the Colebrook-White equation
since it is an implicit relationship for f as a function of Re. The FZERO
function calls a user-defined function to evaluate the particular function of
interest. In this case the implicit function, F(ff), using the Colebrook-White
relationship is coded in an anonymous function Fff (see below).

```

```

File prepared by J. R. White, UMass-Lowell (last update: Nov. 2017)

```

```
clear all; close all; nfig = 0;
```

```
define Re and evaluate the Blasius & Swamee_Jain equations (explicit)
```

```
Re = logspace(4,7,61);
```

```
fB = 0.3164./Re.^(1/4);
```

```
fSJ = 0.25./(log10(5.74./Re.^0.9)).^2;
```

```
now evaluate the Colebrook-White equation (implicit)
```

```
--> use the Swamee-Jain result as an estimate of the root for FZERO.
```

```
NRe = length(Re); fCW = zeros(1,NRe);
```

```
for n = 1:NRe
```

```
    RE = Re(n);
```

```
    Fff = @(ff) 1.0./sqrt(ff) + 0.8 - 2*log10(RE*sqrt(ff));
```

```
    fCW(n) = fzero(Fff,fSJ(n));
```

```
end
```

```
create a table of results
```

```
ratio1 = fB./fCW; ratio2 = fSJ./fCW;
```

```
fprintf(1, '\n      Comparison of Three Friction Factor Correlations for Smooth Pipes \n');
```

```
fprintf(1, '(fB -> Blasius eqn, fSJ -> Swamee-Jain, & fCW -> Colebrook-White correlation)\n\n');
```

```
fprintf(1, '          Re          fCW          fB          fB/fCW          fSJ\nfSJ/fCW\n');
```

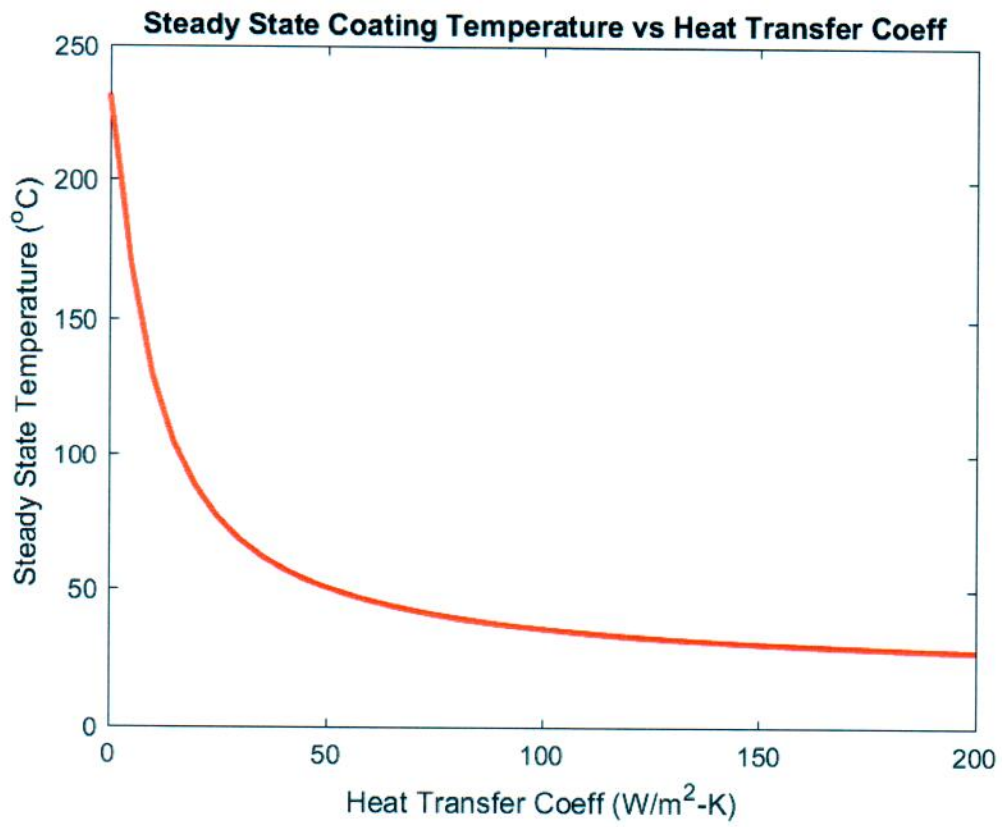
```
for n = 1:2:NRe
```

```
    fprintf(1, '      %10.2e  %8.5f  %8.5f  %8.3f  %8.5f  %8.3f\n', ...
```

```
        Re(n), fCW(n), fB(n), ratio1(n), fSJ(n), ratio2(n));
```

```
end
```

```
% now let's plot the results for easy visualization
nfig = nfig+1; figure(nfig)
subplot(2,1,1),semilogx(Re,fB,'r-',Re,fSJ,'g--',Re,fCW,'b:','LineWidth',2),grid
title('Comparison of three different friction factor correlations')
ylabel('friction factor')
legend('Blasius (B)','Swamee-Jain (SJ)','Colebrook-White (CW)')
subplot(2,1,2),semilogx(Re,ratio1,'r-',Re,ratio2,'g--','LineWidth',2),grid
ylabel('friction factor ratios'),xlabel('Reynolds number')
legend('f_B/f_{CW}','f_{SJ}/f_{CW}','Location','SouthWest')
%
% end of program
```





>> coating\_temp\_1

Summary Results from the COATING\_TEMP\_1.M Program

Basic Design Parameters

Emissivity (dimensionless): 0.50  
Stefan-Boltzmann Constant (W/m<sup>2</sup>-K<sup>4</sup>): 5.67e-08  
Bulk Fluid Temperature (C): 20.00  
Temperature of Surroundings (C): 30.00  
Fraction of Incident Energy Absorbed in Coating: 0.80  
Incident Irradiation from Lamps (W/m<sup>2</sup>): 2000.00

Components of Energy Balance vs. Heat Transfer Coeff.

h (W/m <sup>2</sup> -K)	Generation (W/m <sup>2</sup> )	Convection (W/m <sup>2</sup> )	Radiation (W/m <sup>2</sup> )	Balance (W/m <sup>2</sup> )	SS Temp (C)
0.0	1600.00	0.00	1600.00	0.000	231.55
10.0	1600.00	1094.57	505.43	0.000	129.46
20.0	1600.00	1357.75	242.25	0.000	87.89
30.0	1600.00	1453.41	146.59	0.000	68.45
40.0	1600.00	1500.51	99.49	-0.000	57.51
50.0	1600.00	1528.12	71.88	0.000	50.56
60.0	1600.00	1546.16	53.84	0.000	45.77
70.0	1600.00	1558.82	41.18	0.000	42.27
80.0	1600.00	1568.19	31.81	-0.000	39.60
90.0	1600.00	1575.40	24.60	-0.000	37.50
100.0	1600.00	1581.11	18.89	0.000	35.81
110.0	1600.00	1585.74	14.26	0.000	34.42
120.0	1600.00	1589.58	10.42	0.000	33.25
130.0	1600.00	1592.80	7.20	-0.000	32.25
140.0	1600.00	1595.56	4.44	0.000	31.40
150.0	1600.00	1597.93	2.07	0.000	30.65
160.0	1600.00	1600.00	0.00	0.000	30.00
170.0	1600.00	1601.82	-1.82	0.000	29.42
180.0	1600.00	1603.43	-3.43	0.000	28.91
190.0	1600.00	1604.87	-4.87	0.000	28.45
200.0	1600.00	1606.16	-6.16	0.000	28.03

COATING\_TEMP\_1.M      A Root Finding Example for Steady State Heat Transfer  
 Steady State Coating Temperature on a Plate Exposed to Infrared Irradiation

This file solves for the steady state surface temperature of a flat plate that is irradiated by infrared lamps and that loses energy by both convective and radiation heat transfer. A range of heat transfer coefficients is considered so that a plot of Tss vs h can be made. In this way, one could effectively control the curing temperature of the coating.

The goal of this problem is to illustrate how to solve nonlinear equations using the built-in fzero routine in Matlab. It also demonstrates how, with a simple for loop, to do a parametric study for a single variable -- in this case, we use a range of values of the heat transfer coefficient, h, to show how the steady state curing temperature varies with h. For each value of h, a nonlinear energy balance equation must be solved (here we use fzero to do this) to determine the correct steady state temperature.

A table of results is also produced that shows the various components of the energy balance eqn for each value of h.

Note: When including radiation heat transfer, the computations need to be done using absolute temperatures. Here, however, the final plot and table display temperature in C -- the units conversion is done in the plot and fprintf commands.

The basic idea for this problem comes from Example 1.6 on pgs. 25-27 in the text, Fundamentals of Heat and Mass Transfer, by Incropera and DeWitt 5th Ed (2002, John Wiley & Sons).

File prepared by J. R. White, UMass-Lowell (last update: Nov. 2017)

```
clear all; close all; nfig = 0;
```

```
set parameters for the problem
```

```
emiss = 0.5;                   % emissivity (dimensionless)
sig = 5.67e-8;                % Stefan-Boltzmann constant (W/m^2-K^4)
Tinf = 20+273.15;            % bulk fluid temperature (K)
Tsur = 30+273.15;            % temperature of surroundings for radiation HT (K)
alf = 0.8;                    % fraction of incident energy absorbed in coating
G = 2000;                    % incident radiation from lamps (W/m^2)
```

```
Nh = 41;                      % number of h values to study
htc = linspace(0,200,Nh);    % set range for heat transfer coeff (W/m^2-K)
Tss = zeros(size(htc));       % allocate space for storage of SS temperatures
h = htc(1);                   % h for first value of heat transfer coeff
Tg = Tsur+50;                 % initial guess of Tss for first value of htc
fT = @(T) alf*G - h*(T - Tinf) - emiss*sig*(T^4 - Tsur^4);
Tss(1) = fzero(fT,Tg);        % find actual Tss for first value of htc
```

```
find SS temperautre for each heat transfer coeff (use previous T as guess)
```

```
for n = 2:Nh
  h = htc(n);
  fT = @(T) alf*G - h*(T - Tinf) - emiss*sig*(T^4 - Tsur^4);
  Tss(n) = fzero(fT,Tss(n-1));
```

```

end
%
% plot Tss vs htc
nfig = nfig+1; figure(nfig)
plot(htc,Tss-273.15,'r-','LineWidth',2), grid on
rr = axis; rr(3) = 0; axis(rr);
title('Steady State Coating Temperature vs Heat Transfer Coeff')
xlabel('Heat Transfer Coeff (W/m^2-K)'),ylabel('Steady State Temperature (^oC)')
%
% evaluate components of balance equation (use 'dot arithmetic' where appropriate)
gen = alf*G; % energy rate in by irradiation
conv = htc.*(Tss - Tinf); % loss rate by convection
rad = emiss*sig*(Tss.^4 - Tsur^4); % loss rate via radiation
bal = gen - conv - rad; % SS energy balance eqn
%
% write summary table of results
fprintf(1,'\n\n');
fprintf(1,'          Summary Results from the COATING_TEMP_1.M Program \n');
fprintf(1,'\n');
fprintf(1,'    Basic Design Parameters      \n');
emiss);
fprintf(1,'    Emissivity (dimensionless):           %8.2f    \n',↙
sig);
fprintf(1,'    Stefan-Boltzmann Constant (W/m^2-K^4): %9.2e    \n',↙
Tinf-273.15);
fprintf(1,'    Bulk Fluid Temperature (C):           %8.2f    \n',↙
Tsur-273.15);
fprintf(1,'    Temperature of Surroundings (C):      %8.2f    \n',↙
alf);
fprintf(1,'    Fraction of Incident Energy Absorbed in Coating: %8.2f    \n',↙
fprintf(1,'    Incident Irradiation from Lamps (W/m^2): %8.2f    \n',G);
fprintf(1,'\n');
fprintf(1,'    Components of Energy Balance vs. Heat Transfer Coeff. \n');
SS Temp \n');
fprintf(1,'          h          Generation      Convection      Radiation      Balance↙
(C) \n');
for n = 1:2:Nh
    fprintf(1,'          %5.1f      %8.2f      %8.2f      %8.2f      %8.3f      %8.2f↙
\n', ...
            htc(n),gen,conv(n),rad(n),bal(n),Tss(n)-273.15);
end
%
% end of problem

```